1 High-Throughput Optimization of Paper-Based Cell-Free Biosensors

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6 Abstract

7 Cell-free expression systems maintain core cellular processes without intact cells and offer 8 attractive properties as point-of-need biosensors. The ability to lyophilize, store, and use on-9 demand make these sensors usable in the field, and the lack of membranes means that there 10 are no analyte transport issues and that new sensors can be deployed by simply adding a 11 different DNA molecule. The lack of membranes also means that sensor designs and reaction 12 optimizations can be screened in high throughput. While shelf stability has been demonstrated 13 in specific cases using additives, these approaches are not universal to the myriad cell-free 14 expression methods and formats. Here, we present new high-throughput screening methods to 15 optimize cell-free expression formulations when embedded into paper for use as sensors. Our 16 method leverages acoustic liquid handling to dispense reactions onto 384-well paper ticket 17 formats and machine vision to quantify reaction performance from a colorimetric reporter 18 enzyme. The throughput enabled shifts the bottleneck from experimental execution to selecting 19 the experiments to execute; we therefore implement design-of-experiments to optimize the 20 information gained from each design-build-test-learn cycle. We used these approaches to first 21 optimize the performance of a low-cost cell-free expression formulation that was initially non-22 functional when embedded in paper, then further optimize it for tolerance to exposure to heat. 23 With only 2 rounds of experimentation lasting 4 days total for each goal, the result are an energy 24 mixture with 8% of the materials cost of a commonly used version and a formulation of 25 excipients that maintain 60% of activity after 6 hours of storage at 50 °C and. Finally, we

showcase the use of the cost-optimized formulation in a 3D-printed paperfluidic device where it
outperforms the standard formulation at much lower cost.

28 Keywords

29 Cell-free expression; synthetic biology; biosensors; paper-based sensors; shelf-stability; design

30 of experiments

31 Synthetic biology's increasing use of large datasets has significantly improved the process of 32 repurposing and reengineering natural biological systems towards addressing global 33 challenges. For instance, rewiring molecular biosensors and their associated genetic networks 34 have resulted in simple-to-use and cheap biological diagnostics capable of responding to 35 environmental perturbations dangerous to human health. The use of cell-free expression (CFE) 36 systems enables gene expression from non-living, in vitro biochemical reactions powered by 37 lysed cells and/or purified transcription and translation components combined with mixtures of 38 function-encoding nucleic acids, cofactors, and energy sources^{1,2}. Biological sensors developed 39 from these CFE systems have led to a multipurpose platform capable of sensing a variety of 40 analytes including: pathogen biomarkers, environmental contaminants, and industrial precursors and products ^{3–8}. 41

42 Extending the capability of cell-free biosensors requires that they can effectively be produced, 43 stored, and used in austere and resource-limited environments¹¹. The ability to freeze-dry and 44 embed cell-free biological components into matrices promises to enable their fielddeployability^{9,10}. Cell-free paper sensors address fieldability needs as they can be easy to read 45 46 without external devices when paired with visual reporters, are small and disposable, and can 47 be adapted to different applications by changing the DNA encoding the sensor functionality¹². 48 However, cell-free sensors can be rendered ineffective due to non-ideal conditions such as breaks in cold-chain and reduced access to relevant components¹³. Previous efforts have 49

50 demonstrated methods involving cryoprotectants that enable shelf stability of CFE reactions for 51 months at room temperature and 37°C in non-paper formats^{14–16}; one early study showed ~20% 52 activity after 1 year of storage of CFE reactions on paper without cryoprotectants⁴. The cost of 53 CFE reactions is also an important factor for the technology to reach its potential. While several 54 studies have assessed materials costs, one formulation offers substantially lower cost while maintaining substantial yield¹⁷; until recently, to our knowledge no further published efforts had 55 56 taken advantage of this formulation, and still none have tested it for biological sensors. Beyond 57 cost, disruptions to supply lines due to the COVID19 pandemic impacted the cell-free 58 community as critical components, especially tRNAs, became increasingly scarce to the point of near absence from traditional marketplaces^{18,19}. As a result, developing a low-cost CFE 59 60 formulation that works well on paper and is more resilient to supply chain disruptions would 61 have a substantial impact on the viability of CFE sensors for a range of applications.

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63 Addressing this need benefits from the use of high-throughput testing platforms and 64 methodologies capable of significantly reducing the timeframe for design-build-test-learn (DBTL) 65 cycles²⁰. Previous work using high-throughput methods for aqueous reactions have been shown 66 to effectively improve CFE performance for new organisms, metabolic reactions, and general CFE reaction dynamics^{21–23}. None of these methods have been applied to sensors or reactions 67 68 involving solid matrices like paper; instead, paper sensors have been tested using time- and 69 labor-intensive methodologies, limiting their use as a testing platform. To alleviate this 70 bottleneck, we developed a high-throughput testing platform specifically for reactions on paper 71 and implemented a design-of-experiments (DOE) approach to take advantage of the 72 throughput. DOE allows for systematic exploration and optimization of complex systems by 73 elucidating factors with a significant effect on a desired response; this allows experimenters to 74 determine optimum formulations in a complex system using a fraction of the number of experiments compared to testing one factor at a time or even some machine learning 75

76 methodologies^{20,23-25}. We applied these methods to optimize a low-cost CFE system that was 77 originally inactive on paper to perform on par with standard systems, then optimized additives to 78 improve the stability of CFE sensors to storage at elevated temperatures. With only 2 rounds of 79 experimentation, one exploratory and one predictive, our efforts led to cell-free paper ticket 80 sensors that maintained performance at 8% of the original cost as well as formulations capable 81 of functioning following exposure to 50 °C temperatures for 6 hours. Further, the decreased-cost 82 mixture was found to be more effective than standard mixtures when used in a 3D-printed 83 paperfluidic device.

84 Materials and Methods

85 384-well Ticket Preparation

Wax tickets were printed directly on 1CHR chromatography paper (Whatman) using a Xerox ColorQube printer and prepared for use in the following manner: each ticket was baked at 125 °C for 5 minutes, allowed to cool at room temperature for 5 min, incubated for 1 h in 5% BSA, washed thrice with diH20, and allowed to dry overnight in a fume hood. Paper tickets were stored in fume hood until use.

91 Preparing and Running Cell-Free Reactions

All CFE reactions utilized either a pY71 plasmid with a T7-expressed LacZ insert (pY71-LacZ)
or a combination of two plasmids using the pUCGA vector, one for T7-expression of trH RNA
and the other for T7-expression of swH-lacZ RNA. All DNA was ordered from Aldevron as Giga
Preps.

96 T7 Polymerase Expression Protocol

97 An overnight culture of cells was grown in LB Media with Ampicillin at 37 °C. The next day 500 mL of LB was inoculated with 1 mL of the overnight culture and grown at 37 °C until the OD600 98 99 reached 0.4. Protein expression was induced by adding IPTG to a final concentration of 100 μ M. 100 and the culture was incubated overnight at 37°C. The cells were then pelleted at 5,000 g for 20 101 minutes at 4 °C and resuspended in 25 mL lysis buffer (1/2x PBS, 0.01% Triton X-100, 1 mM 102 EDTA). The cells were lysed by sonication, and the lysate was centrifuged to pellet the cellular 103 debris at 30,000 g for 30 minutes at 4 °C. The supernatant was then transferred to a clean 50 104 mL tube, with 1.0 mL of Ni-NTA purification resin and incubated for 1 hour at 4 °C with shaking. 105 We used 20 mL of wash buffer to clean the resin (50 mM phosphate, 300 mM NaCl, 10 mM 106 imidazole, pH 7.5) and eluted using a gravity flow (50 mM phosphate, 300 mM NaCl, 250 mM 107 imidazole, pH 7.5). Protein-containing fractions were combined and dialyzed in a 3.5k MWCO 108 dialysis cassette against 2L of S30 buffer overnight at 4°C and subsequently at -20 °C.

109 E. coli Lysate Preparation

110 Lysate preparation was carried out using E. coli Rosetta (DE3) AlacZ strains for all experiments. 111 A 100L culture of Rosetta (DE3) AlacZ cells was processed for lysate production similar to the 112 previously described production of BL21(DE3)* lysate, but with modifications to accommodate 113 production at scale. Briefly, 750 mL starter cultures (1.5 L total) were grown for 16 hours at 37°C 114 with 200 rpm shaking incubation. Prior to inoculation, 100 L of 2X YT+P culture media 115 supplemented with 5 mL of antifoam 204 (Sigma, A8311) in an IF 150L (New Brunswick 116 Scientific) fermenter was allowed to aerate overnight with a rotor speed of 100 rpm and 20 117 standard liters per minute (slpm) airflow at 37°C. Following inoculation to a starting OD600 of 118 0.05, the fermenter settings were adjusted to 300 rpm, 50 splm, and the dissolved oxygen (DO) 119 was calibrated to 100%. Upon reaching an OD600 of 0.6-1.0, the culture was induced with a

final concentration of 1 mM isopropyl B-D-1-thiogalatopyranoside (IPTG) (GoldBio, I2481C).
Once DO reached 50%, the rotor speed was increased to 500 rpm. At an OD600 of 3.5, the
culture was cooled to 4°C, centrifuged in a prechilled Powerfuge pilot, 1.1 L bowl system (CARR
Biosystems) within approximately 8 hours, and the pelleted bacteria was subsequently
processed as described previously.

125 Preparing and Running Cell-Free Reactions

126 All CFE reactions utilized either a pY71 plasmid with a T7-expressed LacZ insert (pY71-LacZ) 127 or a combination of two plasmids using the pUCGA vector, one for T7-expression of trH RNA 128 and the other for T7-expression of swH-lacZ RNA. All DNA was ordered from Aldevron as Giga 129 Preps. CFE reactions contained 30% v/v lysate and PANOx-sp or Cai buffer as described in 130 detail previously²⁵. All components and final concentrations are summarized in Table S1-3. After 131 mixing, CFPS reactions were lyophilized in plates, tubes, or vials depending on the scale 132 described for specific experiments. Base CFE reactions were modified with excipients and reagents using working solutions based on each experiment and distributed by Echo liquid 133 134 handler; PANOx-SP, Cai energy mixture, and excipient working solutions found in (Tables S4-135 5). Amounts of additional reagents for the optimized formulations are described in the main text, 136 and Supplementary Data. Paper tickets were prepared for liquid dispensing by directly attaching 137 using adhesive (3M Super 77 Multipurpose Spray Adhesive) to a 384-well Thermofisher 138 microwell plate (Thermofisher Catalog Number: 142761). Reaction components were dispensed 139 directly onto the 384-well ticket using an Echo 525 acoustic liquid handler (Beckman Coulter) or 140 multipipettor for volumes below 1000 nL and above 1000 nL, respectively. Unless otherwise 141 noted all swH/trH tickets were prepared to contain a final concentration of 50 ng/µL pUCGA-trH-142 lacZ per reaction when resuspended in 2uL final volume. The Echo Plate Reformat software 143 and custom scripts were used to prepare Echo transfer protocols. Reactions were lyophilized 144 using a lyophilizer (VirTis AdVantage XL-70, SP Scientific) using a bell jar attachment. The shelf 145 was prechilled to -40 °C, and the condenser to between -65 and -70 °C. The paper tickets were frozen for at least 5 min in a -80 °C freezer. After removing the plate, it was immediately 146 147 placed in the lyophilizer, the vacuum was activated, and the shelf temperature set to -20 °C 148 overnight. The 384-well tickets were prepared for reading by attaching the ticket via adhesive 149 directly to a 384-well plate that had been filled with 30 µL of water per well. Ticket spots were 150 resuspended in 2 µL of 50 ng/µL pUCGA-trH-lacZ DNA in diH20 using a multipipettor unless 151 otherwise noted. Following rehydration, the plates were sealed with a plate cover from a 152 microwell plate (Thermofisher Catalog Number: 142761), the edges wrapped in parafilm to 153 prevent evaporation, and placed directly into a scanner for imaging (see Data Collection and 154 Machine Vision Analysis section).

155 DOE and Statistical Analysis

156 All statistical analyses in this section were performed using Stat-Ease Design-Expert 13 and 157 SAS JMP® Pro 15 software. To optimize the Cai reaction mixture, I-Optimal criterion was used 158 to create optimal Mixture-Amount DOEs based on a guadratic statistical starting model. The 159 design used a starting model that was quadratic on the mixture side and quadratic on the 160 process side, with a "Kowalski-Cornell-Vining" (KCV) structure that restricted the crossing of the 161 mixture and process term (amount) to 2-way. The design is capable of fitting non-linear 162 blending effects up to second order. Within each of the 14 or 16 individual components for 163 adding Cai or PANOx-SP components, respectively, the low and high limits varied by 164 component. Additional details of the DOE models are available in the Supplementary Results 165 and Supplementary Data File.

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For the heat tolerance optimization mixtures, I-Optimal criterion was used to create an optimalMixture DOE based on the quadratic statistical starting model. The Mixture type DOE design

169 was selected in order to maximize experimental efficiency³⁰. A quadratic starting model having 170 the ability to characterize all linear blending effects for each of the individual 14 formulation 171 components as well as all possible non-linear blending effects involving any pair of the 14 172 formulation components was selected. For heat tolerance reactions, a formulation the 14 173 individual components were limited to a range of 0 to 1000 nL. Additionally, each sample 174 formulation was subject to a total volume of 3000 nL.

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176 Functional Data Analysis (FDA) for both case studies was applied via the "Functional Data 177 Explorer" platform within SAS JMP® Pro 15 software. A Functional Principle Components (FPC) 178 decomposition was applied to the response curves, decomposing each curve into a Functional 179 Principle Component "1" (FPC1) and Functional Principle Component "2" (FPC2) score where 180 the FPC1 and FPC2 scores for an individual sample response curve represent the deviation 181 from the overall mean response curve. A statistical model for the DOE generated was then fit to 182 the FPC1 and FPC2 responses. Forward and backward step regression using the Akaike 183 Information Criterion (AiC) was used to reduce the model for the FPC1 and FPC2 response, 184 respectively. The R-Square Predicted metric was used along with the "check-points blends" (in-185 line validation samples) to validate the DOE based prediction models' predictive capability. 186 Optimization was performed using the Stat-Ease Design-Expert 13 Numerical Optimization 187 feature in parallel with the SAS JMP® Pro 15 software Prediction Profiler Platform. Both 188 softwares start with the DOE based prediction model and, after converting the FPC response to 189 a zero to one desirability scale, use numerical methods to find the formulations that best 190 optimize the response.

191 Data Collection and Machine Vision Analysis

192 Image processing from 384-well tickets was performed using three major steps. The ticket is 193 placed on a flatbed scanner (Epson, Perfection V600 Photo) housed within an incubator to 194 produce a time course of sensor images at 37 °C. Each plate is arranged on the scanner at an 195 arbitrary point and scanned directly following rehydration. Custom software was used to capture 196 raw 16-bit color images of the scanner bed at specified intervals. The series of images were 197 then analyzed to monitor the biosensor's response over time using scripts that process the 198 images as follows: time course images are placed in consistent orientation; spots are delineated 199 from the image background and segmented into individual positions (Figure S1): average RGB 200 value for each spot tile is computed; and the color change (ΔE) and hue values (ΔH) returned 201 for each well within the context of CIELAB perceptual color space. For the purposes of this 202 work, an arbitrary point of visibility was designated at $\Delta E=10$ wherein experimenters agreed the 203 color shift was very clear (Figure S2).

204 3D-Printed Sensor Design.

205 All designed parts were created in SolidWorks (SolidWorks) computer aided design software 206 and exported as .stl files for slicing within the Ultimaker Cura software (Ultimaker). "Engineering 207 - Normal" parameters were selected on Cura utilizing support for overhangs greater than 45° 208 and without additionally printed build plate adhesion. Parts were printed using Ultimaker ABS 209 and Ultimaker Breakaway Support filament on the Ultimaker S5 dual extrusion 3D printer. Prior 210 to printing, the glass bed was pre-treated with AirWolf ABS adhesion solution prior to preheating 211 the build plate to 125 °C. All paper layers were printed and prepared as described above prior to 212 the addition of the cell-free extract mix. The agarose-topped layer was prepared by directly 213 adding 5 µL of 1.25% molten agarose to each paper spot. Each extract layer was prepared as 214 described above. Both the cell-free extract layer and the agarose-topped layer were then frozen at -80 °C and lyophilized as described above. Sensors were assembled by placing each layer on the sampling plate, adding a form fitted "quad" top plate over the agarose-topped layer, and covering the top with MicroAmp Clear Adhesive Film (Thermo Fisher). Sensors were tested through the addition of 25 μ L of 50 ng/ μ L pUCGA-trH into the sample chamber and incubating in the flatbed scanner at 37 °C.

220 Results and Discussion

221 High-Throughput Testing Platform of Paper-embedded Reactions

222 Due to the labor-intensive nature of paper-based cell-free biosensor development, we reasoned 223 that the development of a high-throughput testing platform to explore large combinatorial search 224 spaces would accelerate improvement of their overall function. Paper-based reactions in the 225 literature are typically prepared using biopsy punches to cut out small discs that are placed into 226 microtiter plates or wax-printed paper tickets with modest numbers of wells; reactions are then 227 spotted, lyophilized, and rehydrated, typically by hand (Figure 1A)^{26,27}. While this method 228 effectively creates portable sensors, it is not amenable to high-throughput experiments as even 229 simple titrations of fixed reagents create a high-experimental load. For example, a more 230 complex experiment using the excipients in this study to improve durability of a sensor to heat 231 creates a combinatorial search space of 6,103,515,625 potential combinations when using only 232 5 fixed concentrations (Figure 1B). To improve cell-free paper sensors testing throughput, we 233 replicated the commonly used 384-well format using wax-printing on paper, yielding a 234 127.76x85.47 mm 384-well paper ticket template with 3.5 mm diameter wells. Biologically 235 inactive adhesive was used to apply the paper ticket over a standard 384-well plate, and an 236 Echo 525 Acoustic Liquid Handler was used to transfer reaction components from an Echo 237 source-plate to the sensor wells using standard Echo protocols. The tickets were then 238 lyophilized, rehydrated using DNA, and CFE reaction activity measured by color change using a

239 flatbed scanner and custom machine vision and image analysis software, described in detail in

240 the methods, that extracts a measure of human-perceived color change (ΔE) (Figure 1C,





Figure 1: Optimizing paper-based cell-free reactions in high throughput. **A.** Cell-free components are lyophilized directly to a paper disc or ticket and rehydrated with an aqueous analyte to start protein production, in this case LacZ (β -galactosidase), to affect a color change from yellow to purple by cleavage of the CPRG substrate. **B.** An example experiment changing fixed concentrations of salts affecting CFE

(top) and a more complex experiment assessing protective additives with 5 fixed concentrations (bottom). C. Representative image of 384-well wax-printed paper ticket. D. Traces of ΔE from titrations of a plasmid encoding for constitutively expressed LacZ (pY71-LacZ) in the PANOx-SP CFE system extracted from time course images of a ticket. E. Graphic illustration of the DBTL cycle used to explore the combinatorial space of cell-free paper-ticket compositions. Initial tests of excipients and reagents defined an initial DOE matrix that was tested and the resulting data used to define a predictive model for active and optimal reagent concentrations.

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244 Figure 1C shows a representative 384-well ticket with reactions expressing LacZ (β-245 galactosidase), an eye-readable colorimetric reporter that has been used in a wide range of 246 applications²⁸. As an initial validation of the approach, we performed a titration curve of a 247 plasmid (pY71-LacZ) that constitutively expresses LacZ from the strong T7 promoter. For these 248 initial tests, the PANOx-SP formulation was used. The reactions were dispersed onto a 384-well 249 ticket as a master mix with only the plasmid dispersed separately; the ticket was then lyophilized 250 and rehydrated using water. The titration resulted in increasing rates of LacZ production 251 commensurate with the concentration of the DNA transferred, plateauing at 25 ng/µL, which is 252 consistent with prior work indicating a saturation of translational machinery in the CFE reaction 253 $(Figure 1D)^{29}$.

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To explore the vast combinatorial space inherent to non-fixed quanta we decided to employ exploratory DOE with an objective function geared towards improving the rate of our cell-free reactions (**Figure 1D**). The first day of our DBTL cycle is initiated with an exploratory DOE using a list of excipients and additives using volumes ranging from 25 to 1000 nL. The reaction compositions in the exploratory DOE are transferred to the Echo, dispensed on to a 384-well paper ticket, and lyophilized overnight. On the second day, the samples are rehydrated, placed onto a flatbed scanner, color change data extracted, and the resulting data fit to the DOE model.

The loop is then restarted with optimized reaction conditions predicted by the model to be run 262 263 with replicates. DOE offers the ability to efficiently and simultaneously characterize the influence 264 that each formulation component has on the response of interest while at the same time testing 265 for interactions between formulation components and process factors. This is a distinct 266 advantage of DOE experimentation over "one factor at a time" experimentation as we are able 267 to reduce the multidimensionality of the problem to a manageable number of potential test 268 cases. The method allows for large amounts of data to be gathered, analyzed, and fitted to an 269 empirical statistical model that can serve as a prediction for a response at any possible 270 combination of formulation components within the entire design.

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272 Optimization of a Low-Cost CFE Mix

273 As a model diagnostic sensor for the remainder of this work, we used a lyophilized CFE reaction 274 containing a toehold switch plasmid (pUCGA-swH-lacZ) that expresses LacZ in the presence of 275 a target trigger RNA. The biosensor reactions are rehydrated by the addition of a plasmid that 276 constitutively expresses the cognate trigger RNA (pUCGA-trH) (Figure 2A). Lyophilized tickets 277 with identical spots containing 50 ng/µL of pUCGA-swH-lacZ were activated using varying levels 278 of pUCGA-trH (Figure S3). We further tested our ability to dispense reagents by measuring the 279 transfer and subsequent effect of more viscous reagents. RNASE inhibitor has been noted as 280 being important to the function of cell-free paper-based biosensors due to the natural presence 281 of nucleases on the matrix^{10,30}. We titrated the concentration of RNASE inhibitor both to 282 measure the ideal concentration of a critical component and to assess the platform's ability to 283 modulate a viscous reagent. RNASE inhibitor Murine dissolved in 50% glycerol was titrated onto 284 identical CFE reactions, lyophilized, and resuspended in 50 ng/µL of both pUCGA-swH-lacZ and 285 pUCGA-trH. Increasing concentrations of RNASE inhibitor improved the rate of the reaction,

with doubling the typical concentration of RNASE inhibitor to 2.4 units/ μ L providing the best reaction rate and a loss of benefit at 4.8 units/ μ L (**Figure S4**).

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289 A minimized version of the Cytomim CFE system as reported on by Cai and colleagues 290 demonstrated the ability to drop the materials cost of a CFE system by an order of magnitude 291 through the removal of non-essential and expensive components¹⁷. At a total cost of ~\$445/L, 292 the reaction mixture published by Cai heretofore referred to as the Cai reaction mixture is 293 significantly cheaper than the ~\$5,570/L cost of the traditionally used PANOx-SP mixture (Table 294 **S1**)²⁹. This is relevant both for the purposes of making the biosensors affordable in the context 295 of low-resource point-of-need applications and to limit the need for components such as tRNAs, 296 nucleotide triphosphates, and volatile energy sources such as PEP that can be difficult to 297 acquire when supply chains are disrupted. However, we found Cai CFE reactions to produce no 298 clear color change when used with our paper-based biosensors, despite functioning in liquid 299 reactions (Figure 2B). We sought to resolve this limitation as well as reduce the cost per test by 300 optimizing a cheap but inactive-on-paper cell-free energy mixture to function with paper 301 sensors.



Figure 2: Optimization of low-cost CFE reactions for performance in paper-based biosensor reactions. **A**. The presence of trigger RNA disrupts the stem-loop structure of the switch RNA and allows for translation of LacZ (β-galactosidase). **B**. Comparison of PANOx-SP and Cai CFE biosensor reactions in a liquid format in plates; **(inset)** the same reaction components in the paper-based biosensor format after a 3 h

incubation **C.** DOE heatmap produced from the addition of Cai reaction components to the baseline Cai CFE formulation. **D.** Similar experiment was performed using PANOx-SP reaction components added to the baseline Cai formulation. **E.** Heatmap of compositions of the 30 optimal mixtures predicted from DOE analysis. **F.** Time courses of paper tickets using predicted optimized mixtures adding PANOx-SP reagents to baseline Cai mixture. Blue stars indicate the point at which the paper ticket reaction reached $\Delta E \ge 10$. Standard deviations shown as shadows on each trace were derived from triplicate reactions.

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304 We hypothesized that the absence or low concentration of one or more critical components 305 resultant from the cost-minimization efforts was a likely cause of the inability of the Cai to 306 function on paper. To test this hypothesis, we designed a DOE framework to add combinations 307 of components of the Cai formulation by dispensing them directly on 384-well tickets containing 308 normal Cai reactions (Methods). The tickets were then lyophilized to both to normalize the final 309 reaction volumes and because lyophilization is an important aspect of real-world applications of 310 the technology. After rehydration, color change traces were extracted as previously. Though our 311 machine vision approach is capable of quantifying small shifts in color, a threshold of $\Delta E \ge 10$ 312 was used to note a point at which the reactions became obviously visible by eye and served as 313 a barometer for sensor function for the remainder of this study (Figure S2). We prepared an 314 initial 16-component DOE using the components of the standard Cai mix, adding variable 315 amounts of each component in volumes ranging from 0-1000 nL (Figure 2C; Table S5). While 316 some combinations of added reagents did produce detectable signal, the data was not sufficient 317 to fit the DOE model and make predictions of optimal formulations. Following these results, we 318 speculated that some component(s) of the PANOx-SP mix might explain the poor relative 319 performance of the Cai mix compared to PANOx-SP on paper tickets. We next used a 153-320 sample framework adding variable amounts of 14 PANOx-SP components to baseline Cai 321 reactions (Table S4). Many of these combinations showed a marked improvement in the 322 function of the Cai mix on paper sensors (Figure 2D). Additional details about the DOE, data

323 processing, and results are available in the Supplementary Results, Figures S5-7, and
324 Tables S7-8.

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326 Our initial DOE model generated 30 optimal reaction mixtures that spanned diverse 327 combinations of added components (Figure 2E). We test the top 10 predicted optimals and 328 each reached the threshold for visibility within 1.5 hrs, except for Cai-Opt1 which was inactive 329 (data not shown) (Figure 2F). Nine formulations were active and with statistically no difference 330 in speed when compared to the PANOx-SP controls (Table S9). These formulations further had 331 costs ranging from \$0.0013-\$1.96 per 1 µL reaction added to \$0.00044 for baseline Cai; these 332 costs range from ~43-fold cheaper to 35-fold more expensive than the \$0.056 for PANOx-SP, 333 with higher costs driven almost entirely by additional DNA (Table S10). Here we predicted 334 optimal formulations purely based on performance; it is likely that these costs could be driven 335 down further by instead predicting formulations that maximize performance per unit cost.

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337 Analyzing the combinations of additives that result in high performing formulations do not 338 provide simple, obvious intuition into the determinants of improved performance. Notably, all 14 339 components appeared at both the highest and lowest levels in at least one of the 30 predicted 340 optimal formulations, though some do appear more frequently. By considering the blending 341 coefficients for the first and second order effects predicted by the model to have the greatest 342 impact, it is clear that none of the components in isolation explain the improvements in 343 performance (Table S7). The second order effects offer scant additional insight and instead 344 highlight the complexity of the system (Table S8). For example, spermidine appears in 4 of the 345 10 strongest estimated second order effects both as a negative effector (with T7 RNAP and 346 HEPES) and as a positive effector (with RNASE inhibitor and 20 AA Mix). It is worth pointing out 347 that the DOE approach makes no attempt to model the complete system; instead, it aggregates 348 estimates of first and second order effects in a way that can find improved performance after 349 testing only a tiny fraction of a large search space. Moreover, interpretation of the effects of 350 individual components is complicated by the Mixture-Amount design wherein constraints on the 351 total amounts added mean that changing one variable necessitates changing others 352 simultaneously. One noteworthy observation is that the model estimates that RNASE inhibitor 353 provides a positive effect in combination with Spermidine, CoA, and PEP, but a small negative 354 effect alone, suggesting that our earlier conclusion that additional RNASE inhibitor improves the 355 reaction for the PANOx-SP system is dependent on one or more specific components in the 356 mix. Ultimately, despite providing limited insights into the inner workings of the system, the 357 model reliably predicted diverse, high-performing formulations. Until mechanistic models are 358 developed that can fully capture the highly complex dynamics of CFE reactions, DOE offers a 359 powerful tool to rapidly optimize formulations for a particular use case.

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361 Engineering Cell-Free Biosensor Heat Tolerance

The need for biosensors in austere environments inherently requires that the biological systems are capable of functioning outside ideal laboratory conditions. For instance, high salt, temperature, or pH environments can deactivate biological sensors. These problems can be magnified if the tools in question require notoriously difficult to maintain cold chains. We sought to improve the robustness of our sensors to elevated temperatures during storage through the addition of excipients with previously reported impacts on the function of lyophilized products following exposures to environmental stresses (**Table S6**).

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During the sublimation process, the disruption of hydrogen bonding pairs can result in protein aggregation. To resolve this issue, excipients are often added to purified protein components in order to stabilize electrostatic complexes during drying. Additionally, exposure to temperatures

373 above a protein's melting temperature can unfold regions with thermodynamically unfavorable 374 refolding and lead to aggregation and ultimately inactivity of the biosensor. Preliminary 375 experiments with paper biosensors using the PANOx-SP system exposed to 6 hr incubation at 376 50 °C were found to be completely inactive (data not shown). We hypothesized that an effective 377 combination of excipients to improve heat tolerance could be found by applying a DOE analysis 378 to the lyophilization and heat testing process. We produced a DOE matrix testing combinations 379 of 14 excipients shown to provide protective effects in other studies^{15,32–35} by adding them to the 380 baseline PANOx-SP system and measuring the activity following heat challenges. An initial 6 hr 381 incubation at 50 °C showed several reactions with a substantial improvement in the heat 382 tolerance (Figure 3A).

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Figure 3. Cell-free biosensors were tested for improved activity following heat exposure using various excipients to improve performance. **A.** Heatmap of activity of DOE-generated combinations of lyophilization excipients to the baseline PANOx-SP CFE mix after exposure of lyophilized tickets to 50 °C for 6 hr. **B.** Heatmap of additive volumes for the 30 optimal mixtures predicted from DOE. **C.** Traces of predicted optimal mixtures following heat exposure. The exploratory graph shows the average time course of the active reactions from the exploratory experiment. The top 14 predicted optimal formulations were tested. Blue star indicates time to $\Delta E \ge 10$. Standard deviations shown as shadows on each trace were derived from triplicate reactions.

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Unlike the prior optimization, there were clear trends in the components that appeared in 386 387 predicted optimal formulations: some excipients (e.g. PEG, lactose, and rhamnose) appeared 388 rarely or not at all in the predicted top formulations, while others (e.g. H₂KPO₄, Ficoll, and 389 Raffinose) appeared frequently (Figure 3B). Considering the linear and non-linear blending 390 coefficients for the model, however, again yields a complicated picture (Tables S11-12). For 391 example, while PEG, lactose, and rhamnose had relatively strong negative linear effects, 392 PEG+rhamnose and lactose+rhamnose had relatively strong positive effects. This observation 393 is explained by how the coefficients are weighted to predict the FPC1 value according to our 394 Mixture-Amount constraints. More specifically, component amounts are pseudo-coded to range 395 from 0 to 0.333 such that no single component can go above 1000 nL out of a maximum 396 allowed 3000 nL total amount. For the example of PEG, lactose, and rhamnose added at 397 maximum amounts, the predicted FPC1 value is calculated as:

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$$399 \quad \text{FPC1}_{\text{Predicted}} = \frac{1}{3} \sum_{\substack{\text{PEG,} \\ \text{lactose,} \\ \text{rhamnose}}} \text{Linear blending coefficients} + \frac{1}{9} \sum_{\substack{\text{PEG,} \\ \text{lactose,} \\ \text{rhamnose}}} \text{Non-linear blending coefficients}$$

$$400 \qquad \qquad = \frac{1}{3}(-248.4 - 290.8 - 126.1) + \frac{1}{9}(0 + 1453.4 + 1158.8) = 68.5$$

401

Since 68.5 is much low compared to the predicted optimals (e.g. #30 is predicted at 205.3), this apparent discrepancy is clarified. This observation can be interpreted as PEG, lactose, and rhamnose each having negative effects alone, with rhamnose having synergistic effects with both PEG and lactose that do not overcome the negative individual effects. While deeper insights into how these complex formulations perform would be highly welcome, as discussed above, the purpose of the DOE approach is to predict optimal formulations despite limited understanding of the system.

409

410 Fourteen predicted optimal formulations along with the top performing formulation from the 411 exploratory DOE were further tested in quadruplicate by exposing the tickets to a 6 h incubation 412 at 50 °C (Figure 3C). Notably, several of these reactions appeared to perform favorably to 413 untreated PANOx-SP samples from the Cai optimization experiments (Figure 2F), though we 414 did not include that control to enable a direct comparison. We nonetheless checked the 415 statistical significance of these apparent improvements (run on different tickets on different 416 days) and found no significant difference in time to reach a $\Delta E \ge 10$ for any of the optimal 417 formulations compared to PANOx-SP, which is unsurprising given substantial variability 418 between replicates (Table S11; see discussion on variability below). While the Heat-Opt11 419 formulation reached the ΔE threshold for visibility at 47 min, the best reported in this study, it is 420 not clear if the additives truly improved the performance of the base PANOx-SP. While we did 421 not further explore the performance impact of these additives without heat exposure, other work 422 has noted the dual purpose of maltodextrin as a lyoprotectant and energy source, suggesting 423 that such improvements are possible.

424

425 Following our success optimizing the low-cost extract and improving the heat tolerance of our 426 paper ticket sensors, we sought to merge the two-systems by evaluating the effect of adding the 427 heat tolerance excipients optimized for the expensive PANOx-SP reaction mixture to our 428 optimized Cai formulations. We chose 4 optimized Cai formulations (Cai-Opt3 and 9 that use 429 minimal added DNA and Cai-Opt1 and 4 that add maximum DNA) and 2 optimized heat-430 tolerance formulations (Heat-Opt 11 and 13 for the fastest mean time to $\Delta E \ge 10$) and exposed 431 pairwise combinations of these formulations on tickets to 50 °C for 0, 3, or 6 h (Figure 4 and 432 Tables S9, S13). We found that even without heat exposure, all combinations except the two 433 involving Cai-Opt9 performed poorly but were still active; after heat exposure those 434 combinations performed progressively worse, with four of the six combinations never reaching

435 $\Delta E \ge 10$ after 6 h exposure to 50 °C. Both combinations involving Cai-Opt9, however, performed 436 similarly to the earlier PANOx-SP controls (mean time to $\Delta E \ge 10$ of 80, 90, and 96 min for 437 PANOx-SP, Heat11+Cai9, and Heat13+Cai9, respectively), and retaining some activity after 438 heat exposure (mean time to $\Delta E \ge 10$ ranging from 152 to 184 min). Further work would likely 439 uncover combinations that provide better heat tolerance while maintaining low costs.



Figure 4. Heat tolerance of combinations of optimized Cai formulations and heat-tolerance excipient combinations optimized using PANOx-SP as the baseline. Combinations of Cai-Opt1, 3, 4, and 9 and Heat-Opt11 and 13 were added to baseline Cai on tickets and exposed to 50°C for 0, 3, or 6 h. Shaded error bars are one standard deviation from n=4 replicates. A blue star indicates the time at which the cell-free biosensor reached a ΔE of 10; if no replicates reached the threshold, a value of 0 is shown.

441 Handheld Biosensors Effectively Make use of Optimized CFPS Mixtures

442 To showcase the effectiveness of our optimized reactions, we designed and created a handheld

443 paperfluidic device to show the potential of the colorimetric sensor as a diagnostic tool. A 4-

444 layer wax-printed paperfluidic sensor housed in a 3D-printed cassette (Figure 5A, Figure S8) was built using either the unoptimized Cai mix, PANOx-SP, or an optimized version of the Cai 445 446 mix (Cai+Opt4) and tested by flowing pUCGA-trH plasmid through the device. As expected, the 447 Cai mixture without optimization did not produce any detectable result, whereas both the 448 PANOx-SP and the optimized Cai reaction mixtures were all visible within 42 minutes (Figure 449 **5B-C**). Interestingly, the optimized Cai mixtures led to a faster time to visibility than the standard 450 PANOx-SP system ($\Delta E \ge 10$ at 26 vs 42 mins, respectively; p=0.034), becoming statistically 451 differentiable at 32 min (p<0.05). These reaction times outpace the 384-well ticket apparatus 452 $(\Delta E \ge 10 \text{ at } 80 \text{ vs } 88 \text{ min for PANOx-SP and Cai-Opt4, respectively; Figure 2F}), indicating that$ 453 the handheld biosensor system improves the function of the CFE reaction both in general and 454 differentially for the optimized formulation. Notable differences are sealing of the device to limit 455 evaporation and the presence of an agarose-hydrogel layer intended to enhance flow in the 456 paperfluidic system. Given that hydration of the reaction mixture can be crucial to function, both 457 of these factors likely help to maintain an environment more amenable to the CFE reactions³¹. 458 This observation shows the importance of the physical and environmental factors that can 459 modify the function of cell-free biosensors and opens new avenues for further research and 460 development. Rehydration, dilution of the components, and variable environmental humidity and 461 temperature have all been shown to be critical factors, especially in the context of biological 462 sensing³⁶. This work further incentivizes context-specific modifications for biological sensing 463 platforms as directly porting one reaction mixture to a different context can have unintended consequences. 464



466 Figure 5. Performance of optimized biosensors in a fieldable paperfluidic device. A. Schematic of a wax-467 printed paperfluidic device wherein sample is added to the sample layer, disseminated using a paper 468 fluidic layer to the individual reaction chambers containing cell-free extract, and visualized on an agarose-469 topped layer held together by a 3D printed holder (Figure S8). The "*" indicates a sample chamber with 470 a CFE reaction and pUCGA-swH-lacZ; "+" indicates a positive control containing a CFE reaction with both 471 pUCGA-swH-lacZ and pUCGA-trH plasmids; "-" indicates a negative control containing a CFE reaction 472 with no DNA; and "e" being an empty node intended to identify any leaking between layers. Both the top 473 and bottom layer 3D-printed enclosures are sealed with transparent film following sample addition. B. 474 Assembled sensor devices were imaged and analyzed using the same scanning rig and software as 475 above. C. Time courses of three replicate devices. The shadow indicates one standard deviation. Blue 476 stars indicate time to cross ∆E≥10. One tailed T-test shows statistically significant difference compared to 477 negative controls at 32 min for Cai-Opt4 and PANOx-SP sample reactions.

479 Assessment of Variability

480 In the initial tests of our experimental platform titrating pY71-LacZ plasmid, we observed 481 reasonably consistent error bars (Figure 1D). In later cases, however, we found that error bars 482 for replicate experiments were larger, resulting in a lack of statistical significance between conditions even when differences in means appear large, e.g. the previously discussed 483 484 differences between the heat-tolerance optimal formulations and PANOx-SP. We therefore 485 assessed the CV of time to $\Delta E \ge 10$ across all data sets (Figure 6). We found that the initial 486 pY71-LacZ titrations were anomalously consistent (CV=6.9%) compared to other 384-well ticket 487 experiments (CV=28.0-39.5%). Previous efforts to measure variability of CFE reactions has 488 found that ~6-10% is typical for a single experimenter across days when prepared by hand, 489 suggesting that the substantial increase in variability is a result of small volume dispensing 490 errors either from the acoustic liquid handler or baseline master mixes. More careful calibration 491 and validation of proper dispensing would be needed to validate this hypothesis and 492 subsequently mitigate any issues. Other possibilities are that time to $\Delta E \ge 10$ using an enzymatic 493 reporter is more variable than the endpoint GFP fluorescence used in the other studies or that 494 something about the paper ticket format increases variability; however, because in one case we 495 saw similar consistency, we suspect dispensing errors are more likely to be the cause. While 496 such variability limits fine tuning of reaction compositions, our results show that rapid, efficient 497 screening through very large combinatorial design spaces is still viable. We note also that the 498 average variability in our device format was 11.2%, indicating that optimal formulations can 499 perform reasonably consistently in a more applied setting.



501

502 **Figure 6:** Variability within replicates across experiments in this study. Bars represent the average within-503 replicate CV across each experiment list. Error bars represent one standard deviation.

504

505 Conclusions

506 Scaling the production of cell-free biological sensors requires cost-effective and stable methods 507 of producing them as diagnostic tools. This work shows how high throughput experimentation 508 driven by DOE can rapidly identify substantial improvements in performance at low costs and with tolerance to heat exposure in paper formats relevant to application. Given the complexity of 509 510 these formulations, traditional optimizations varying one or two variables at a time are 511 intractable; with the approaches outlined here, a single researcher can reduce enormous search 512 spaces to a manageable number of experiments that can be executed in two consecutive days. 513 The ability to then immediately port these improvements into a fieldable diagnostic device from 514 low-cost, easy-to-produce components underscores the potential for such sensors to have real 515 world impact. We anticipate that continued development of new CFE sensors paired with further

- 516 improvements to the performance, cost, stability, and deployability of CFE reactions will lead to
- 517 the technology achieving its potential impact.
- 518

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524 Author Contributions

- 525 DCG: Conceptualization, Methodology, Investigation, Data curation, Writing Original Draft;
- 526 JPD: Methodology, Formal analysis; CED: Software; DAP: Methodology; AEM: Methodology,
- 527 Supervision; MWL: Conceptualization, Writing Review & Editing, Supervision, Project
- 528 administration, Funding acquisition.

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531 532

Supplemental Information

533 High-Throughput Optimization of Paper-Based Cell-Free Biosensors

534

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540 Supplementary Results

541 Design of experiments

542

543 Compressing data with Functional Principal Component analysis

544

545 In order to fit the DOE models described above, the curves were first decomposed into 546 Functional Principal Components (FPC). Results of the FPC decomposition of DOE for adding 547 PANOx-SP components to baseline Cai are described in this section. After an initial FPC 548 decomposition, we plotted the FPC1 scalars to identify any systematic issues (Figure S7). The 549 experimental design is such that output should be randomly distributed across the samples, so 550 any observed patterns indicate potential issues. Of the first 17 samples, 16 had minimal activity. 551 We expect that this anomaly arose from a dispensing error by the acoustic liquid handler. 552 Because the anomaly was systematic, we excluded samples 1-17 from further analysis. This 553 anomaly further raises the question of other potential dispensing errors that do not result in an 554 obvious systematic error. While we do not rule out this possibility, we note that DOE methods 555 are generally robust to experimental errors.

556

557 After removing the outliers, we found that 94.8% of the variation could be explained by a single

558 Eigenfunction (FPC1) representing a generic sigmoid shape (Figure S8). A second

559 Eigenfunction (FPC2) explains an additional 4.85% of variation by dampening the slope of the

response and introducing a positive slope to the plateau. Because FPC1 alone explains the data well, we used the FPC1 scalar as our fit metric.

561 dat 562

563 An alternative choice to using FPC1 as the design objective would be to use the time until 564 $\Delta E \ge 10$. Since our goal is to create fast sensors, this alternative choice would be more direct; 565 however, the use of FPC1 does indirectly select for response time by maximizing the linear 566 scaling of FPC1 without discarding additional information about curve shape. To check what 567 impacts the choice of a different objective function might have had, we re-ran the DOE analysis with time to $\Delta E \ge 10$ as the objective. We found that the profile of median amount of each 568 569 component added was similar across the top 10 predicted optimals, suggesting that the search 570 space represented by each set of predicted optimals is likely similar (Figure S9). Since little 571 difference was observed, we chose to proceed with FPC1 as our objective function because of 572 our anticipated-but-unverified notion that capturing the full curve information can help mitigate 573 the impact of outliers.

574

575 Descriptions of DOE models used

576

577 The initial design for this experiment was a screening design intended to identify whether components of the Cai formulation could be added to recover activity of baseline Cai reactions. 578 579 A guadratic Mixture Amount design with 16 components and a single process factor, labeled 580 "Total Volume", was used (Supplementary Data Files). The process factor allowed for variation 581 in the total number of droplets dispensed across all components added to the base Cai reaction. 582 Because the reactions are then lyophilized, we do not expect this process factor to play a significant role in the predictive model. A Quadratic starting model was used with a "KVC" cross. 583 584 This design is I-Optimal and capable of fitting non-linear blending effects up to second order and 585 interactions with the "Total Volume" factor up to 2-way. This design models the influences of the 586 relative ratios of the 16 components as well as the "Total Volume". Despite identifying some 587 combinations that yielded a response, the high number of non-responsive formulations resulted in an ability of the DOE model to fit the data using a backward (BiC) reduced statistical model. 588 589

590 The second attempt mirrored the first except 14 components from the PANOx-SP formulations

591 were added instead, as described in the main text. The detailed design is available in the

592 **Supplementary Data Files**. The resulting data was adequate for fitting the DOE model. A

593 backward (BiC) reduced statistical model was fit to the FPC1 data. The resulting model 594 (R^2 =0.6848, p<0.0001) had 34 terms including linear effects for the 14 reaction components and

595 20 additional non-linear blending effects that were influential enough to be included in the

596 model. These effects and their blending coefficients are detailed in **Table S7-8**. These effects

597 are interpreted in the main text.

598

599 The DOE for heat tolerance followed the same approach except 14 excipients were added to

baseline PANOx-SP reactions. Details of the DOE is available in the **Supplementary Data**

601 These effects and their blending coefficients are detailed in **Table S11-12**. These effects are

again interpreted in the main text.



605 **Figure S1:** Representative example of 384-well CFE paper ticket analysis software extracting color 606 change information for individual wells.

	0	0	0	0	0	0	0	0	0	0	0	0		0
Time (min)	0	0	18	18	38	38	52	52	58	58	60	60	78.4	78.4
ΔΕ	0.0	0.0	-0.7	0.1	-0.8	0.46	-0.7	4.2	-0.8	8.8	-0.71	10.6	-0.4	24.2

608 609 Figure S2: A representative image of the color change over time in a cell-free biosensor using a

610 colorimetric reporter. Though a perceivable color change is seen earlier, we chose ∆E≥10 as a threshold 611 at which the color change is obvious.

612





Figure S3: A PANOx-SP CFPS reagent mix was prepared with the same amount of pUCGA-swH-LacZ 616 plasmid directly added before lyophilization and activated by resuspending using various concentrations 617 of the commensurate trH. The blue star indicates the point at which a ∆E≥10 was reached. Standard

618 deviations shown as shadows on each trace were derived from quadruplicate reactions.



Figure S4: Effect of increasing amounts of RNASE Inhibitor added to the reaction mixture.







629 630 **Figure S6:** Functional Principal Component decomposition of curves resulting from DOE of adding

PANOX-SP components to baseline Cai reactions. (A) Raw traces of ΔE over time extracted from images.
(B) Mean and standard deviation functions of the full data set after removal of outliers. (C) Results of FPC analysis.





Figure S7: Median volumes of each component added in the predicted optimal formulations based on

637 optimizing for FPC1 (top) or time to $\Delta E \ge 10$ (bottom).



- 640 directly to the sampling port and visualized on the surface layer covered in transparent film.

644 Table S1: Cost comparison of CFE reactions using Cai and PANOx-SP formulations. Media

645 calculations assume 300 mL per L, and 3 mL of lysate made per L of media.

	Cai	PA	NOx-SP
Media Components for Lysate			
Tryptone	\$ 77.10	\$	77.10
Yeast Extract	\$ 34.80	\$	34.80
NaCl	\$ 3.41	\$	3.41
Potassium phosphate, monobasic	\$ 10.75	\$	10.75
Potassium phosphate, monobasic	\$ 10.26	\$	10.26
DTT	\$ 87.41	\$	87.41
CFE Components			
YNB	\$ -	\$	-
HEPES	\$ -	\$	5.79
Tris	\$ -	\$	-
Potassium Phosphate	\$ 0.16	\$	-
ATP	\$ -	\$	40.67
GTP	\$ -	\$	302.40
CTP	\$ -	\$	227.61
UTP	\$ -	\$	469.13
AMP	\$ 6.52	\$	-
GMP	\$ 3.54	\$	-
CMP	\$ 17.57	\$	-
UMP	\$ 5.57	\$	-
Oxidized glutathione	\$ 5.69	\$	-
Tyrosine	\$ 0.12	\$	-
PEP	\$ -	\$2	142.72
NAD	\$ -	\$	728.32
СоА	\$ -	\$	681.80
Potassium Glutamate	\$ 16.01	\$	10.78
Ammonium Glutamate	\$ -	\$	0.62
Magnesium Glutamate	\$ 8.62	\$	17.25
Sodium/Potassium Oxalate	\$ 0.05	\$	0.05
Putrescine	\$ -	\$	0.70
Spermidine	\$ 5.05	\$	5.05
Alanine	\$ 0.11	\$	0.11
Arginine	\$ 0.13	\$	0.13
Asparagine	\$ 0.20	\$	0.20
Aspartic acid	\$ 0.03	\$	0.03
Cysteine	\$ 0.19	\$	0.19
Glutamic acid	\$ 0.02	\$	0.02
Glutamine	\$ 0.16	\$	0.16
Glycine	\$ 0.02	\$	0.02

	Total:	\$4	44.97	\$5	,570.37
T7 RNA polymerase		\$	56.40	\$	282.00
DNA Template		\$	92.03	\$	92.03
E. coli tRNA		\$	-	\$	246.58
Folinic Acid		\$	-	\$	89.25
Valine		\$	0.12	\$	0.12
Tyrosine		\$	0.26	\$	0.26
Tryptophan		\$	0.31	\$	0.31
Threonine		\$	0.25	\$	0.25
Serine		\$	0.15	\$	0.15
Proline		\$	0.13	\$	0.13
Phenylalanine		\$	0.19	\$	0.19
Methionine		\$	0.11	\$	0.11
Lysine		\$	0.99	\$	0.99
Leucine		\$	0.15	\$	0.15
Isoleucine		\$	0.25	\$	0.25
Histidine		\$	0.17	\$	0.17

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Table S2: Energy mixture components for PANOx-SP base reactions.

Component	PANOx-SP Final Concentration
Magnesium	12 mM
Potassium glutamate	130 mM
Ammonium glutamate	e 10 mM
Magnesium acetate	3.7 mM
Potassium acetate	6.2 mM
Tris acetate	5.67 mM (pH 8.2)
HEPES	7.5 mM (pH 7.4)
ATP	1.2 mM
GTP	0.85 mM
СТР	0.85 mM
UTP	0.85 mM
Folic acid	0.072 mM
tRNA	170.6 µg/mL
Alanine	2 mM
Arginine	2 mM
Histidine	2 mM

Lysine (monoHCl)	2 mM
Aspartic acid	2 mM
Glutamic acid	2 mM
Isoleucine	2 mM
Leucine	2 mM
Methionine	2 mM
Phenylalanine	2 mM
Tryptophan	2 mM
Tyrosine	2 mM
Valine	2 mM
Serine	2 mM
Threonine	2 mM
Asparagine	2 mM
Glutamine	2 mM
Cysteine	2 mM
Glycine	2 mM
Proline	2 mM
PEP	33 mM
NAD	0.33 mM
CoA	0.27 mM
Spermidine	1.5 mM
Putrescine	2 mM
Oxalic acid	4 mM
T7 RNA polymerase	100 µg/mL
Plasmid DNA	6.4 nM
RNase Inhibitor	1.2 U/µL
Cell extract	30% v/v
DTT	0.5 mM

Table S3. Energy mixture components for Cai base reactions.

Component	Concentration
AMP	1.2 mM
UMP	0.86 mM
СМР	0.86 mM
GMP	0.86 mM
T7 RNA Polymerase	0.02 mg/mL
Magnesium Glutamate	8 mM
Potassium Glutamate	260 mM
Potassium Oxalate	4 mM
Potassium Phosphate pH 7	.015 mM
Spermidine	1.5 mM
Oxidized Glutathione	2 mM
Alanine	2 mM
Arginine	2 mM
Histidine	2 mM
Lysine (monoHCl)	2 mM
Aspartic acid	2 mM
Glutamic acid	2 mM
Isoleucine	2 mM
Leucine	2 mM
Methionine	2 mM
Phenylalanine	2 mM
Tryptophan	1 mM
Tyrosine	2 mM
Valine	2 mM
Serine	2 mM
Threonine	2 mM
Asparagine	2 mM
Glutamine	2 mM

Cysteine	2 mM
Glycine	2 mM
Proline	2 mM
Cell extract	30% v/v
RNase Inhibitor	1.2 U/µL

- Table S4 Working solutions used in energy mixture components for PANOx-SP reagent additives.

Reagent	Concentration
Salt Solution (SS)	10X
HEPES	1 M
Cell-Free Master Mix (MM)) 15X
AA Mix	50 mM
PEP	1 M
NAD	20 mM
CoA	20 mM
Oxalic Acid	250 mM
Putrescine	62.5 mM
Spermidine	62.5 mM
T7 RNAP	1.3 mg/mL
RNASE inhibitor Murine	4 units/µL
Extract	~30 mg/mL
CPRG	-
DNA (each plasmid)	400 ng/µ1

Table S5: Working solutions used in energy mixture components for Cai reagent additives.

Reagent	Concentration
L-Glutamic acid hemimagnesium salt tetrahydrate	40 mM
L-Glutamic acid monopotassium salt monohydrate	e 1300 mM
AMP	25 mM
GMP	25 mM
UMP	25 mM
CMP	25 mM
Oxalic Acid	150 mM
L-Glutathione oxidized	50 mM
Spermidine	125 mM
Potassium phosphate (K ₂ HPO ₄)	307.5 mM

Potassium phosphate (KH ₂ PO ₄)	192.5 mM
Amino Acids (19)	25 mM
Tyrosine	25 mM
T7 RNAP	1.3 mg/mL
RNASE inhibitor Murine	-
Lysate	~30 mg/mL
CPRG	-
DNA (each plasmid)	400 ng/µl

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669 Table S6: Excipients tested for heat tolerance.

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Excipient	Concentration	Role	Reference
Dextran 70	50 mg/mL	Cryoprotectant	Hagen et al. (1997)
PEG8K	5%	Lyoprotectant	Manning et al. (2010)
Maltose	50 mM	Cryoprotectant	Chirife et al. (2000)
H2KPO4	50 mM	Buffering agent	Pikal-Cleland et al. (2000)
Ficoll	50 mg/mL	Cryoprotectant	Wang et al. (2006)
Maltodextrin	50 mM	Bulking agent	Patel and Pikal (1996)
Raffinose	50 mM	Cryoprotectant	Wang et al. (2006)
Lactose	50 mM	Cryoprotectant	Wang et al. (2006)
Rhamnose	50 mM	Cryoprotectant	Chirife et al. (2000)
Mannitol	50 mM	Cryoprotectant	Wang et al. (2006)
Sucrose	50 mM	Cryoprotectant	Wang et al. (2006)
Malitol	50 mM	Cryoprotectant	Wang et al. (2006)
Sorbitol	50 mM	Cryoprotectant	Chirife et al. (2000)
TMAO	50 mM	Stabilizer/Protectant	Wüstner and Solanko (2015)

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672 673 Table S7: Linear blending coefficients from the DOE model of PANOx-SP components added to baseline

Cai. Positive coefficients indicate an increase in FPC1 as the proportion of the component changes.

Linear Blending Coefficient	Name
133.6	1 M HEPES pH 7.4
124.7	Oxalic Acid (250(250mM)
117.1	SWH(400ng/μl)
88.7	T7 RNA (1.3 mg/mL)
70.1	CoA(20mM)
61.2	15x MM
44.6	Putrescine (62.5 mM)
23.3	NAD (20mM)
10.9	Extract
-2.7	Spermidine (62.5mM)
-21.8	10 X SS
-23.9	20 AA Mix (50mM)

-115.2	RNASE inhibitor
-151.5	PEP (1000mM)

- 677 Table S8: Non-linear blending coefficients from the DOE model of PANOx-SP components added to
- baseline Cai. Positive coefficients indicate an increase in FPC1 as the proportion of the componentchanges.
- 679 (680

Non-linear	Component Names
Coefficient	
1,654.40	Spermidine (62.5mM)*RNASE inhibitor
1,173.80	CoA(20mM)*RNASE inhibitor
1,027.40	PEP (1000mM)*RNASE inhibitor
901.2	20 AA Mix (50mM)*Spermidine (62.5mM)
522.3	10 X SS*SWH(400ng/µl)
330.2	PEP (1000mM) * Extract
242	10 X SS*PEP (1000mM)
17.9	PEP (1000mM) * amount (total added)
6.7	Extract *amount (total added)
-45.1	SWH(400ng/µl)*amount (total added)
-72.8	Putrescine (62.5 mM) * amount (total added)
-196.2	1 M HEPES pH 7.4*Extract
-383	1 M HEPES pH 7.4 *PEP (1000mM)
-628.6	15x MM *CoA(20mM)
-967.3	1 M HEPES pH 7.4*Spermidine (62.5mM)
-1,361.90	15x MM*Oxalic Acid (250(250mM)
-1,541.70	CoA(20mM)*Oxalic Acid (250(250mM)
-1,565.00	1 M HEPES pH 7.4 * SWH(400ng/µl)
-2,299.30	Putrescine (62.5 mM) * SWH(400ng/µI)
-2,708.30	Spermidine (62.5mM)* T7 RNA (1.3 mg/mL)

- 683 **Table S9:** Results of independent t-tests performed to compare the PANOx-SP controls against each
- 684 experimental dataset when ΔE≥10 for the optimized Cai formulations. The p-values assess the statistical
- 685 significance of these differences using n=4 samples.

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Comparison	p-value
Cai+Opt1	0.415247
Cai+Opt2	0.650334
Cai+Opt3	0.256598
Cai+Opt4	0.816178
Cai+Opt5	0.871965
Cai+Opt6	0.96559
Cai+Opt7	0.252361
Cai+Opt8	0.407565
Cai+Opt9	0.735271

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Table S10: Cost breakdown of Cai optimized formulations. Costs are given per 1 µL reaction.

Index	Cai-Opt Costs	Baseline Cai Cost	Total Cost per Reaction
1	\$ 1.95876	\$ 0.00044	\$ 1.95920
2	\$ 0.00129	\$ 0.00044	\$ 0.00173
3	\$ 0.00133	\$ 0.00044	\$ 0.00177
4	\$ 1.96275	\$ 0.00044	\$ 1.96320
5	\$ 0.00132	\$ 0.00044	\$ 0.00177
6	\$ 0.00131	\$ 0.00044	\$ 0.00176
7	\$ 0.49299	\$ 0.00044	\$ 0.49343
8	\$ 1.96420	\$ 0.00044	\$ 1.96465
9	\$ 0.00141	\$ 0.00044	\$ 0.00186
10	\$ 1.95528	\$ 0.00044	\$ 1.95573
11	\$ 0.00021	\$ 0.00044	\$ 0.00065
12	\$ 0.49558	\$ 0.00044	\$ 0.49603
13	\$ 0.49721	\$ 0.00044	\$ 0.49766
14	\$ 0.00022	\$ 0.00044	\$ 0.00067
15	\$ 1.95924	\$ 0.00044	\$ 1.95968
16	\$ 0.00259	\$ 0.00044	\$ 0.00303
17	\$ 1.95974	\$ 0.00044	\$ 1.96018
18	\$ 0.00255	\$ 0.00044	\$ 0.00300
19	\$ 0.49694	\$ 0.00044	\$ 0.49738
20	\$ 0.50248	\$ 0.00044	\$ 0.50293
21	\$ 0.49139	\$ 0.00044	\$ 0.49184
22	\$ 1.96049	\$ 0.00044	\$ 1.96094
23	\$ 1.95581	\$ 0.00044	\$ 1.95625
24	\$ 1.96259	\$ 0.00044	\$ 1.96304
25	\$ 1.47543	\$ 0.00044	\$ 1.47588
26	\$ 0.00316	\$ 0.00044	\$ 0.00361

27	\$ 1.96094	\$ 0.00044	\$ 1.96138
28	\$ 0.00442	\$ 0.00044	\$ 0.00487
29	\$ 0.97770	\$ 0.00044	\$ 0.97814
30	\$ 1.96160	\$ 0.00044	\$ 1.96204

- 692 **Table S11:** Linear blending coefficients from the DOE model of heat tolerance excipients added to
- 693 baseline PANOx-SP. Positive coefficients indicate an increase in FPC1 as the proportion of the
- 694 component changes.
- 695

Linear Blending Coefficient	Component Name	
258.4	Raffinose 50mM	
170.5	Maltose 50mM	
136.9	Ficoll 50mM	
132.4	TMAO 50mM	
131.2	Maltodextrin 50mM	
72.3	Sorbitol 50mM	
33.5	Н2КРО4	
18.8	Dextran 70 50 mM	
-62.6	Sucrose 50mM	
-107.8	Mannitol 50mM	
-126.1	Lactose 50mM	
-135.7	Malitol 50mM	
-248.4	PEG5%	
-290.8	Rhamnose 50mM	

- 698 **Table S12:** Non-linear blending coefficients from the DOE model of heat tolerance excipients added to
- 699 baseline PANOx-SP. Positive coefficients indicate an increase in FPC1 as the proportion of the

700 component changes.

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Non-linear	Component Names
Blending	
Coefficient	
1580.7	Dextran 70 50 mM*Mannitol 50mM
1453.4	PEG5%*Rhamnose 50mM
1203.2	Sucrose 50mM*Malitol 50mM
1158.8	Lactose 50mM*Rhamnose 50mM
1136.7	Maltodextrin 50mM*Sucrose 50mM
1119.7	H2KPO4*Ficoll 50mM
996.2	Mannitol 50mM*Malitol 50mM
751.6	H2KPO4*Raffinose 50mM
669.2	Ficoll 50mM*Rhamnose 50mM
389.6	Maltose 50mM*Malitol 50mM
-443.1	Dextran 70 50 mM*Malitol 50mM
-659.5	PEG5%*Sucrose 50mM
-729.5	Dextran 70 50 mM*Ficoll 50mM
-735.3	Maltose 50mM*Ficoll 50mM
-750.8	Maltose 50mM*H2KPO4
-853.5	Maltose 50mM*Maltodextrin 50mM
-1038.9	Raffinose 50mM*Sorbitol 50mM
-1100.2	Maltodextrin 50mM*TMAO 50mM
-1120.1	Maltose 50mM*TMAO 50mM
-1423.1	Ficoll 50mM*Rhamnose 50mM

- 704 Table S13. Results of independent t-tests performed to compare the point where of ∆E≥10 for PANOx-SP
- 705 dataset from the Cai optimization experiment against the heat optimized formulations (Heat-Opt1 through

Heat-Opt14). The p-values assess the statistical significance of these differences using n=4 samples.

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Comparison	p-value
PANOx-SP vs Heat-Opt1	0.94
PANOx -SP vs Heat-Opt2	0.99
PANOx -SP vs Heat-Opt3	0.96
PANOx -SP vs Heat-Opt4	0.98
PANOx -SP vs Heat-Opt5	0.83
PANOx -SP vs Heat-Opt6	0.96
PANOx -SP vs Heat-Opt7	0.99
PANOx -SP vs Heat-Opt8	0.97
PANOx -SP vs Heat-Opt9	0.79
PANOx -SP vs Heat-Opt10	0.97
PANOx -SP vs Heat-Opt11	0.97
PANOx -SP vs Heat-Opt12	0.97
PANOx -SP vs Heat-Opt13	0.92
PANOx -SP vs Heat-Opt14	0.87

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